On the Crucial Role of Wind-Wave-Tunnel Studies to Reveal the Mechanisms of Air-Sea Gas Exchange

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Major challenge since half a century

Large uncertainty in gas transfer velocity and the parameters controlling it

- Wind is major driving factor, but
- Energy input split into generating shear current and wind-wave field
- $\bullet \rightsquigarrow$ Turbulence generation by shear flow and breaking waves
- Bubbles submerged by breaking waves generate additional exchange surface
- All these processes are influenced by surfactants at water surface





Field experiments

Recent collection of field data





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Viscous, thermal, and mass boundary layers on both sides





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Basic scales for exchange across air-water interface I

• Speed of exchange: transfer velocity k [cm/h]

$$k = \frac{j}{\Delta C} = \frac{j}{c_{ws} - c_{wr}} \quad (2 - 70 \,\mathrm{cm/h}) \tag{1}$$

• Vertical spatial scale: mass boundary layer thickness z_{\star} [μ m]

$$j = -D \left. \frac{\partial c}{\partial z} \right|_{0} = -D \frac{\Delta c}{z_{\star}} \quad \rightsquigarrow \quad z_{\star} = \frac{D}{k} \quad (350 - 10 \,\mu\text{m}) \tag{2}$$



Basic scales for exchange across air-water interface II

• Temporal scale time constant t_{\star} [s]

$$t_{\star} = \frac{z_{\star}}{k} = \frac{D}{k^2} \quad (60 - 0.06 \, s) \tag{3}$$

• Horizontal spatial scale time constant x_{\star} [m] (footprint required)

$$x_{\star} = \Delta u t_{\star} \quad (100 - 1 \,\mathrm{cm}) \tag{4}$$

Relevant is not advection but velocity difference Δu caused by the shear current within the viscous boundary layer



Active thermography: Spatiotemporal response at 2.0 m/s wind speed



 $\begin{array}{ccc} 0.5\,s & 1.0\,s & 1.5\,s \\ \text{Time after switching on heat flux with CO_2 laser in marked areas} \\ & \text{image sector $25\,cm} \times 25\,cm \end{array}$



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Active thermography: Spatiotemporal response at 2.0 m/s wind speed



 $\begin{array}{ccc} 2.0\,s & 2.5\,s & 3.0\,s \\ \mbox{Time after switching on heat flux with CO_2 laser in marked areas} \\ \mbox{image sector $25\,cm$} \times 25\,cm \end{array}$



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Same at medium wind speed (7.0 m/s)



 $\begin{array}{ccc} 0.5\,\text{s} & 1.0\,\text{s} & 1.5\,\text{s} \\ \text{Time after switching on heat flux with CO_2 laser in marked areas} \\ & \text{image sector $25\,\text{cm}$} \times 25\,\text{cm} \end{array}$



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Imaging of concentration fields within mass boundary layer





No wind, convection induced (left oxygen, right heat) (from Kunz, Bachelor thesis, 2011)



Imaging of concentration fields within mass boundary layer



Imaging of concentration fields within mass boundary layer





Large Heidelberg Annular Air-Sea Interaction Facility (Aeolotron)







Outlook with Preliminary Results At Low and Very High Wind Speeds

- Insoluble hexadecanol monolayer and 5 ppm Triton X-100 completely suppress wind-wave generation up to 8 m/s wind speed
- In contrast, 2.4 g/L hexanol reducing surface tension to 43 dyn/cm does not suppress wind-waves at all
- No visible difference in spatio-temporal structures of concentration fields with monolayer of hexanol and 5 ppm Triton X-100





Hexadecanol Monolayer at \approx 4 m/s Wind Speed







5 ppm Triton X-100 at \approx 4 m/s Wind Speed







Switching Wind Off





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Air-Sea Gas Exchange Lab Studies





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Very High Wind Speeds: New Regime beyond 35 m/s





Very High Wind Speeds DMS and CO₂





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Conclusions

- Novel imaging techniques directly reveal mechanisms of air-sea gas transfer
- Large annular facility provides sufficiently realistic oceanic conditions
- A physically-based model will emerge from the novel approach within two years including the effects of sea state, unsteady winds and surfactants





Extra Material



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Air-Sea Gas Exchange Lab Studies

Modeling Bubble-induced Gas Transfer I

• Bubbles provide additional closed exchange surface

$$k_{\rm tot} = k_s + k_c \tag{5}$$

• Limiting case of low solubility: like open surface

$$k_{c,\text{low}\alpha} = k_{c,600} \left(\frac{600}{Sc}\right)^{n_b} \tag{6}$$

ullet Limiting case of high solubility: bubble carries gas with volume flux Q_b

$$k_{c,\text{high}\alpha} = \frac{1}{\alpha} \frac{Q_b}{A_s} = \frac{k_r}{\alpha} \tag{7}$$

Transfer velocity $\propto k_r = Q_b/A_s$ and to $1/\alpha$; does not depend on Schmidt number



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Modeling Bubble-induced Gas Transfer II

• Exponential transition between the two limiting cases

$$k_{c} = \frac{k_{r}}{\alpha} \left[1 - \exp\left(-\frac{\alpha}{\alpha_{t}}\right) \right] \quad \text{with} \quad \alpha_{t} = \frac{k_{r}}{k_{c,600}} \left(\frac{Sc}{600}\right)^{n_{b}}$$
(8)

• Limiting k_{tot} for clean water ($n = n_b = 0.5$)

$$k_{\text{tot}} = \begin{cases} \left(k_{s,600} + k_{s,600}\right) \left(\frac{600}{Sc}\right)^{0.5} & \alpha \ll \alpha_t \\ \\ k_{s,600} \left(\frac{600}{Sc}\right)^{0.5} + \frac{k_r}{\alpha} & \alpha \gg \alpha_t \end{cases}$$



Just two parameters for bubble-induced gas exchange: $k_{c,600}$ and k_r



(9)

Verification of Model with Multi-Tracer Measurements

from two high wind speed facilities: Kyoto and SUSTAIN (Krall et al., 2019)



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