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A Comparative Study of Oxygen Transfer Over Contracted and **Uncontracted Weirs**

Introduction

- Aeration is a process that introduces air into the water, thereby increasing its dissolved oxygen content.
- The dissolved oxygen concentration is a key indicator of water quality, and a minimum of 4 ppm is essential for maintaining a healthy aquatic ecosystem.
- The water released from hydroelectric power plants usually has very low dissolved oxygen concentration, so aeration becomes necessary.
- In today's scenario, water bodies like rivers and lakes are often polluted, and aeration can play a rejuvenating role in restoring their health.
- The aeration process involves creating turbulence in the water, which can be achieved through hydraulic structures like weirs.
- These structures generate turbulence when water plunges over them and strikes the pool below, effectively carrying air into the pool, thereby increasing dissolved oxygen levels.

Methodology

- The storage tank was filled with tap water and deoxygenated to 1 to 2 ppm by adding a calculated amount of sodium sulphite (Na₂So₃) and cobaltous chloride ($CoCl_2.6H_2O$) as catalyst (Tiwari et al., 2023).
- The disoolve oxygen was measured using HACH DO meter.
- The air concentration was measured using phase detection probe.



Fig. 1: Experimental setup and instruments

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Governing E

• Fick's law describes the mass transfer volatile gas like oxygen from air to wat $\int \frac{dc}{dt} = -K_l a \left(C_s - C \right)$ **Initial Condition** At t = 0, $C = C_{\mu}$ integrating Eq. (1) from time t=0 to t=t, or $\int_{C_u}^{C_d} \frac{dc}{C_s - C} = -K_l a \int_0^t dt$ $\ln \frac{C_s - C_d}{C_s - C_u} = -K_l \text{at}$ $C_t = C_s - (C_s - C_o)e^{-K_L at}$ $r = \frac{(C_s - C_d)}{(C_s - C_u)} = exp(K_Lat)$ E = 1 - - $E = \frac{(C_d - C_u)}{(C_s - C_u)}$ $1 - E_{20} = (1 - E)^{1/f}$ $f = 1 + 0.02103 (T - 20) + 8.261 \times 10^{-5} (T)$ Eq. (8) can be used to calculate the temperature of 20 °C. C_{s} = saturation concentration $C_d = D/S$ concentration $C_{\prime\prime} = U/S$ concentration K_L = liquid film coefficient a = specific interface area E = aeration efficiency at any temperature E_{20} = aeration efficiency at standard temperature = temperature correction factor



Fig. 2: Variation of aeration efficiency

er rate, and the mass transfer of ter can be expressed as: [1]	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$
one gets: [2] [3] [4] [5] [6] [7] [8] $(-20)^2$ [9] aeration efficiency at standard	 ^{0.02} Linear (Q=10 L/s) ⁰ ⁵ ¹⁰ ¹¹ ¹⁰ ¹⁰
e T berature 20 °C	 The aeration efficie The aeration efficie The aeration efficie The aeration efficie Significant air entration The mean air concert The maximum air from entrapment point
S $ \begin{array}{c} \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ $	APHA, AWWA, WEF. (2) Waste Water, APHA Was Gulliver, John S., and Ala hydraulic structures." Jou Gulliver, John S., John R aerated flows." Journal o Kim, Jeongkon, and Richa of Environmental Engine Lewis, Warren K., and W & Engineering Chemistry Nakasone, Hideo. "Study engineering 113.1 (1987)





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Fig. 4: Air concentration profile

- n of aeration efficiency with jet width of weir where B is B_w is the total width of weir
- ncreases with splitting of jet because of jet interaction and
- n of aeration efficiency with drop height, the aeration eigh drop height because the mlore is the height more is the
- centration profile of a jump which forms when jet from weir sulting in high air entrainment and oxygen transfer.

Conclusions

ency of contracted weir is more than uncontracyted. ency decreases with increase in flow rate. ency increases with increase in drop height. ainment was observed near the jump toe. ntration was also found to be higher at jump toe. concentration decreased with increase in distance int.

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