

Experimental and modeling assessment of slug tests in the presence of coupled hydraulic, thermal, and solute transport effects

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Curriculum Vitae



Xiaosong Dong

Education Background

Hohai University Politecnico di Milano (CSC scholarship)

2022-Present: Doctoral degree (ongoing) Ranking: Top 2/11

2020-2022: Master's degree Ranking: Top 1/49

2016-2020: Bachelor's degree Ranking: Top 5/77

Major: Geological Resource and Geological Engineering

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Research Achievements

✓ Publication:

seven papers in English
ten papers in Chinese

✓ Patents:

nine invention patents

✓ Research Projects:

more than ten research projects

Selected Honors & Awards

✓ National Scholarship (Top 1%)

✓ Outstanding Student Leader (Top 1%)

✓ Outstanding Graduates (Top 5%)

✓ Outstanding Presenter/Student (Top 10%)

✓ Academic Excellence Scholarship (Top 10%)

✓ Sci&Tech Innovation Scholarship (Top 10%)

✓ First class Postgraduate Scholarship (Top 30%)

Internship & Activities

✓ Student Membership of CSRME

✓ Alumni Liaison Staff of Hohai University

✓ Vice President of Graduate Student Association

✓ Secretary General of the Student Self-Management Committee



CONTENT

1. Research Background

2. Laboratory Model

3. Theory and Methods

4. Conclusion



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Research Background



1. Research Background



hydrogeological
parameters

Multi-field
coupling

slug tracer
test

- ① There are still many problems in the comprehensive determination of hydrogeological parameters in aquifers;
- ② Slug test is known for its small impact area and easy operation;
- ③ Tracer test is used to determine the dispersion coefficient of an aquifer;
- ④ Multi-field coupling is an extremely complex problem

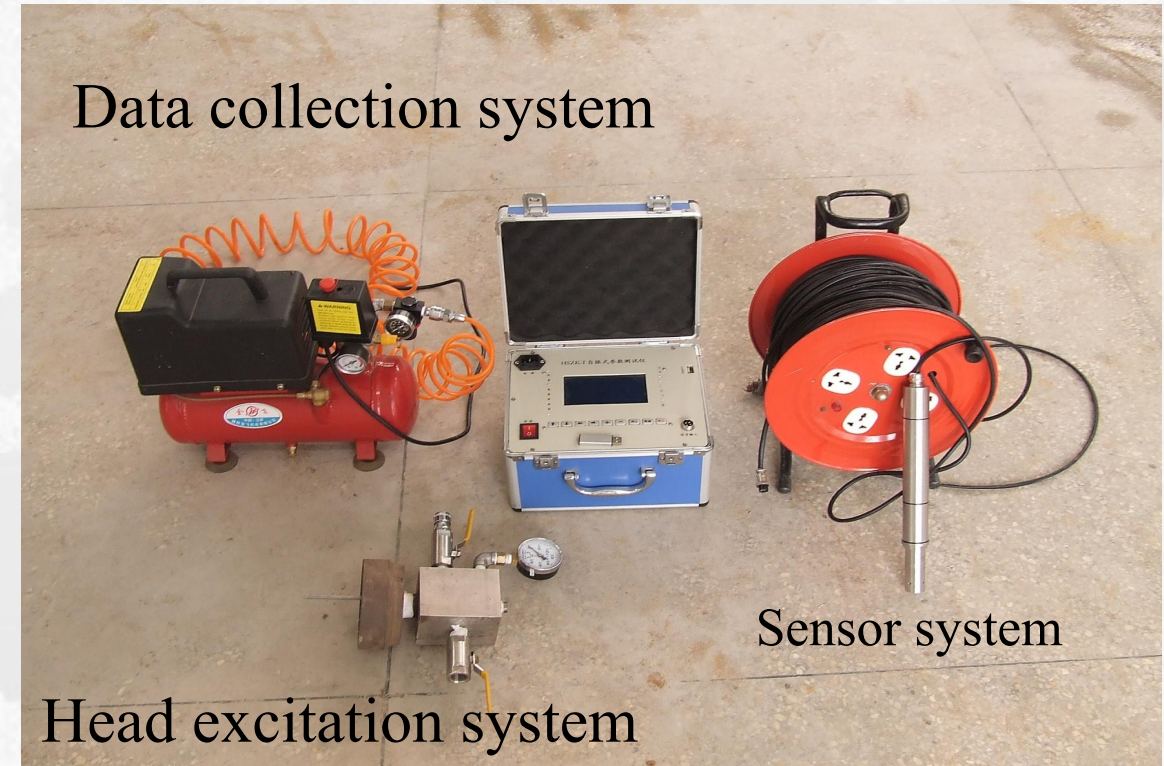


1. Research Background



Slug Test

- (1) Slug tests use a single well for the determination of aquifer
- (2) Rather than pumping the well for a period of time, a volume of water is suddenly removed or added to the well casing and observations of recovery or drawdown are noted through time
- (3) Slug tests are often preferred at hazardous waste sites, since no contaminated water has to be pumped out and then disposed.



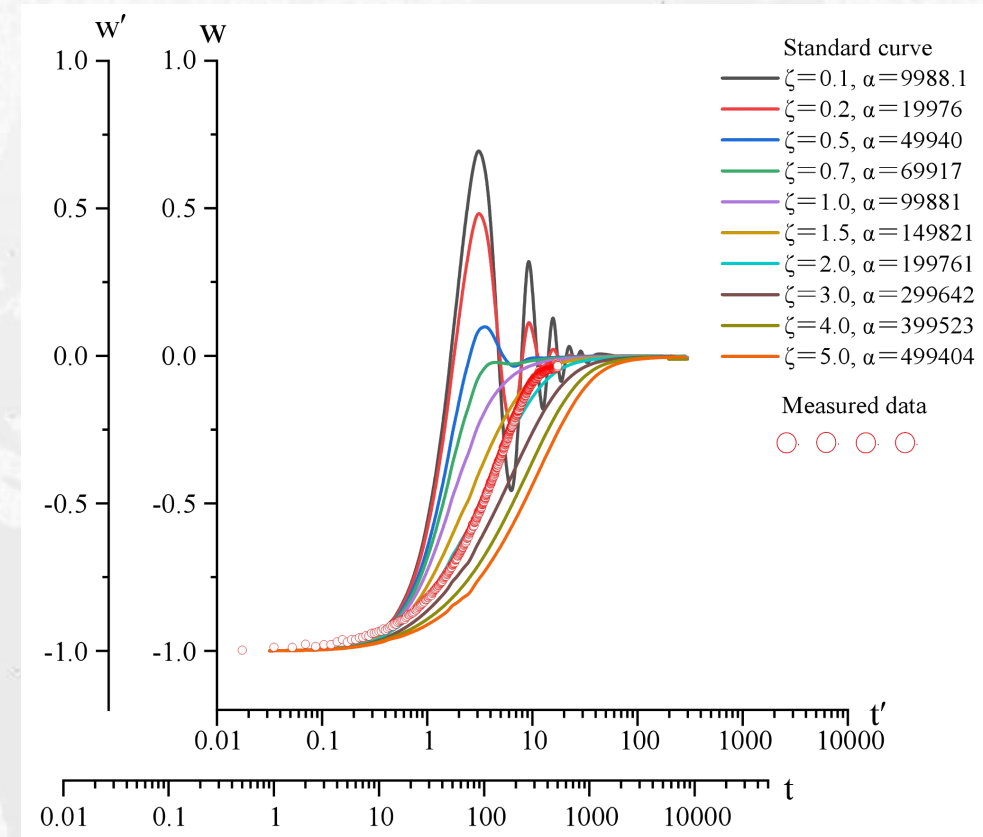
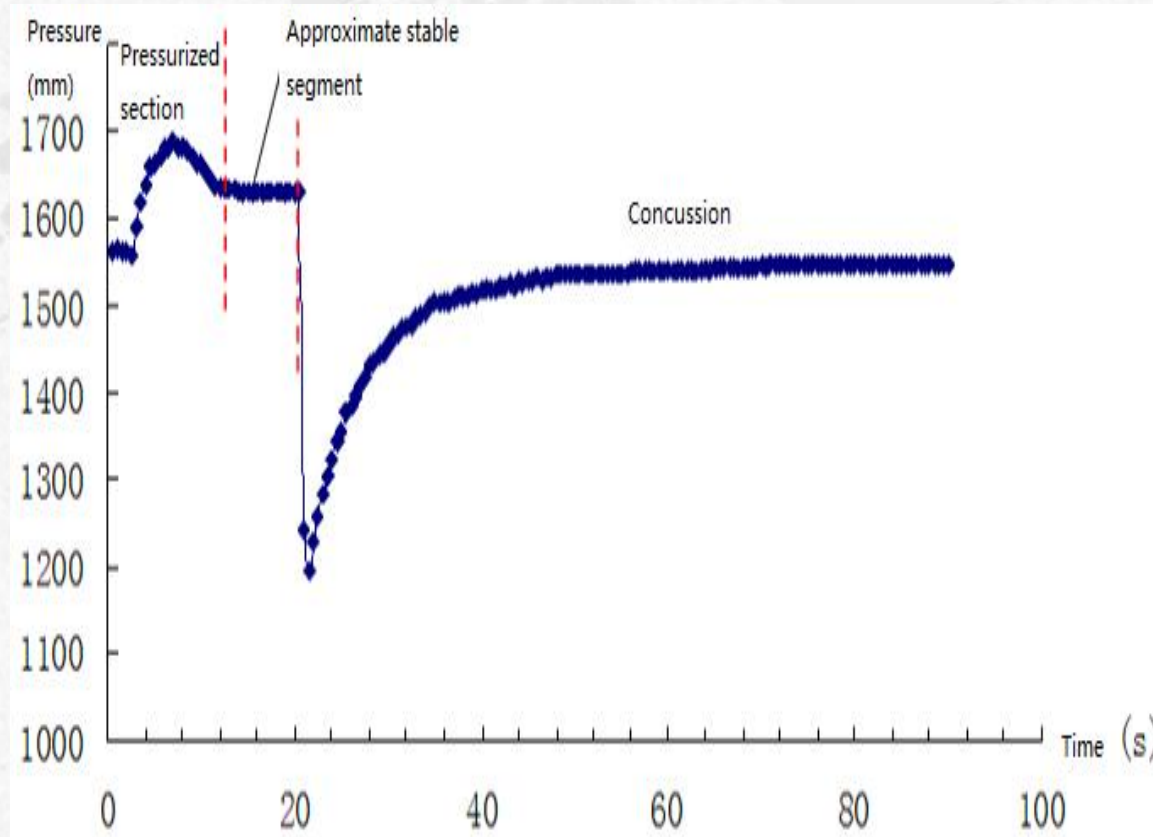
Pictures of the slug test system



1. Research Background



Slug Test

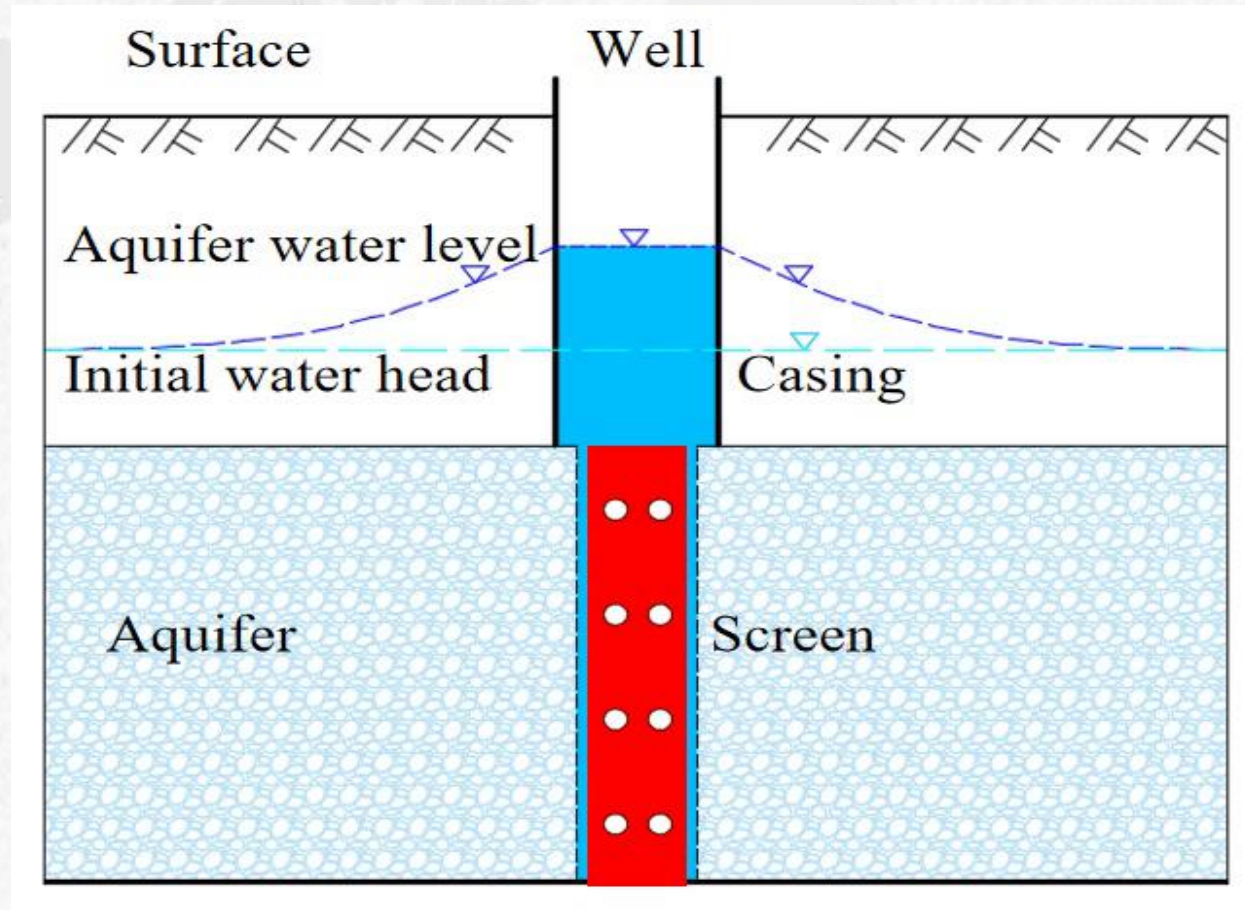


Measured curve & standard curve of slug test



1. Research Background

slug heat test



Experience model studies



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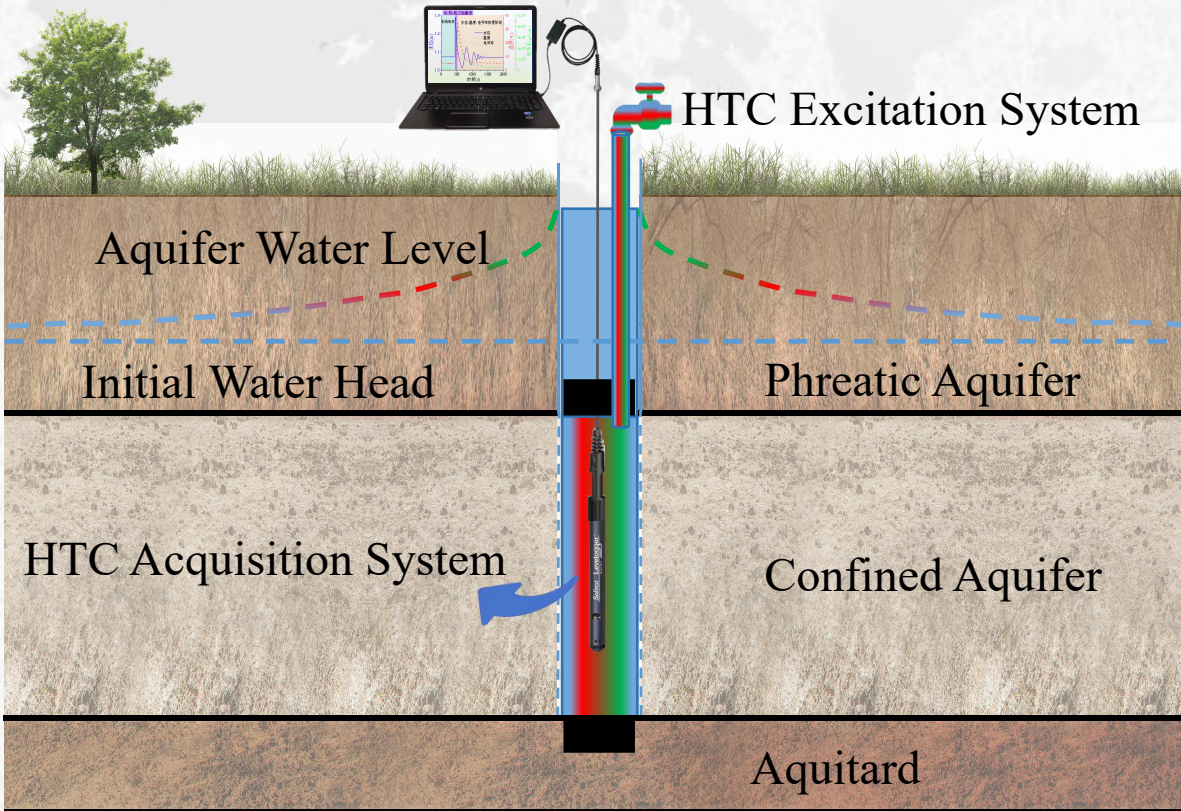
Laboratory Model



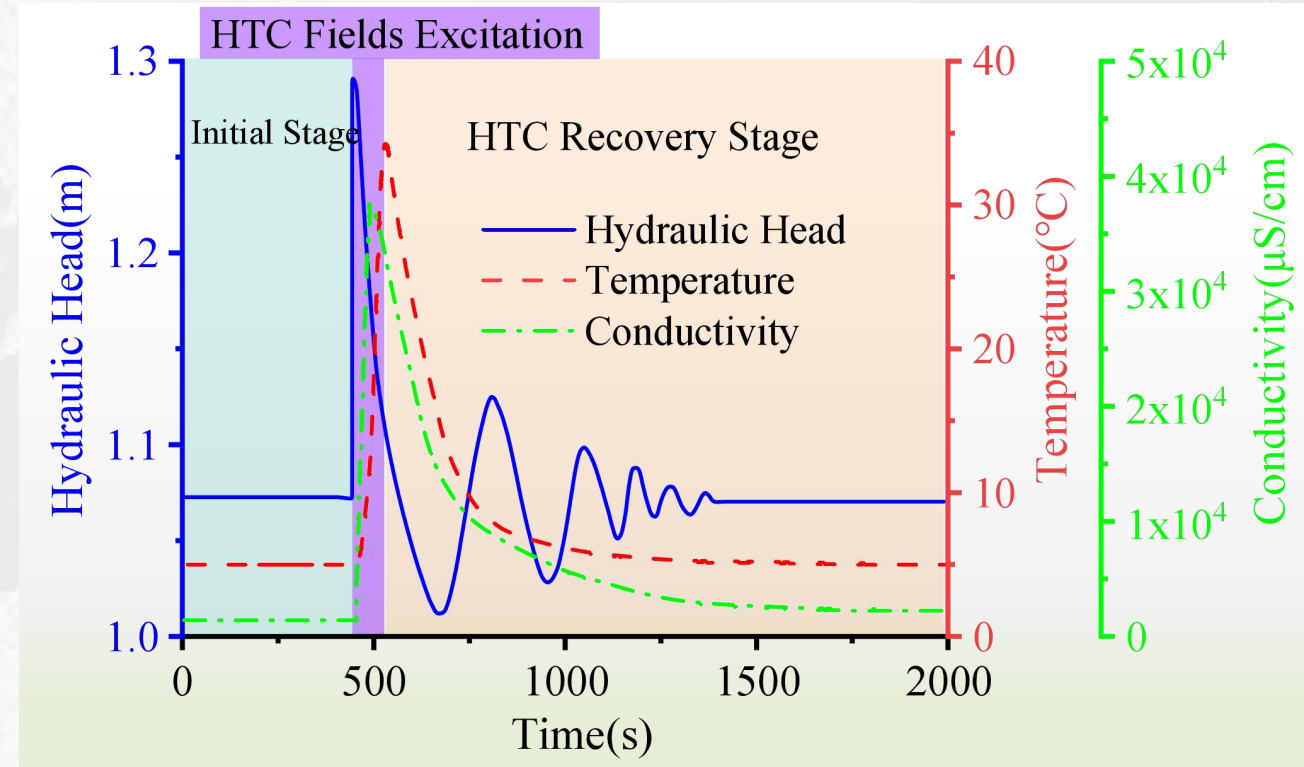
2. Laboratory Model



Hydraulic-Thermal-Chemical Fields Coupling



Experimental Schematic Diagram



Schematic Diagram of Experimental Data



2. Laboratory Model



HTC Probe



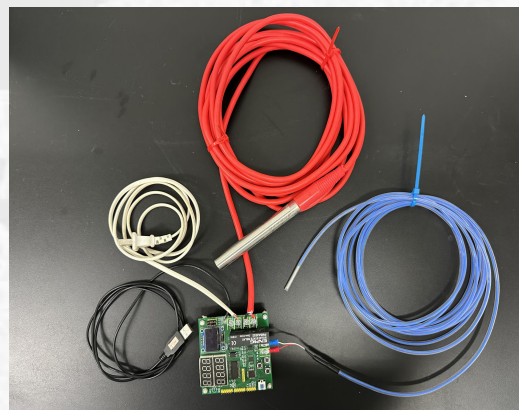
Data Transmitter



Data Cable



Peristaltic Pump



Heating Rod



Digital Screen

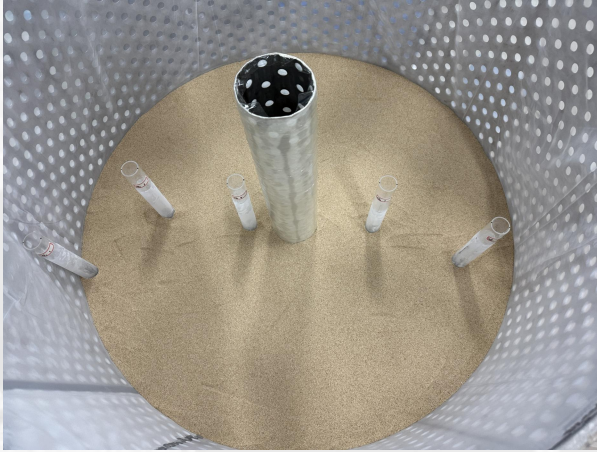
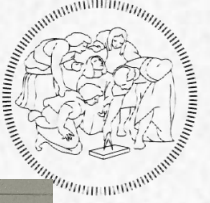


**Overall Diagram
of Platform**

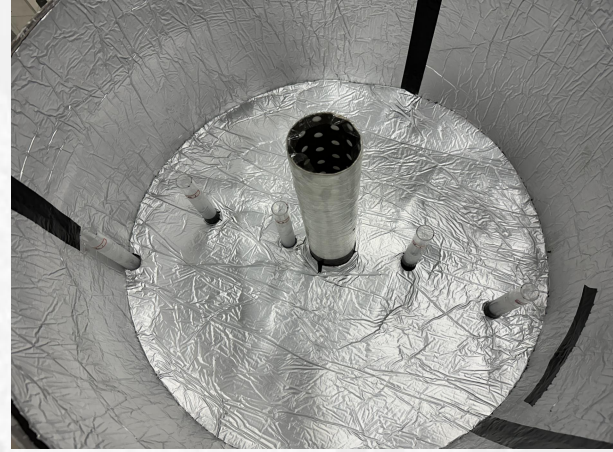
One-dimensional Experimental Platform



2. Laboratory Model



Sand Filling



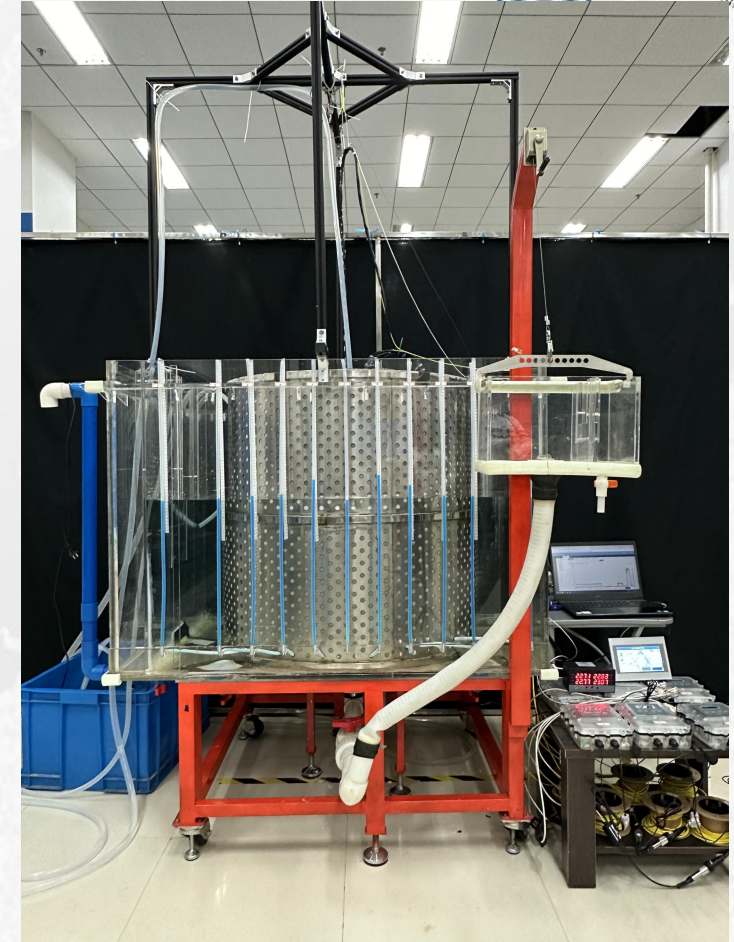
Heat Protection Film



Cement Filling



Top View



Front View

Two-dimensional Experimental Platform



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Theory and Methods



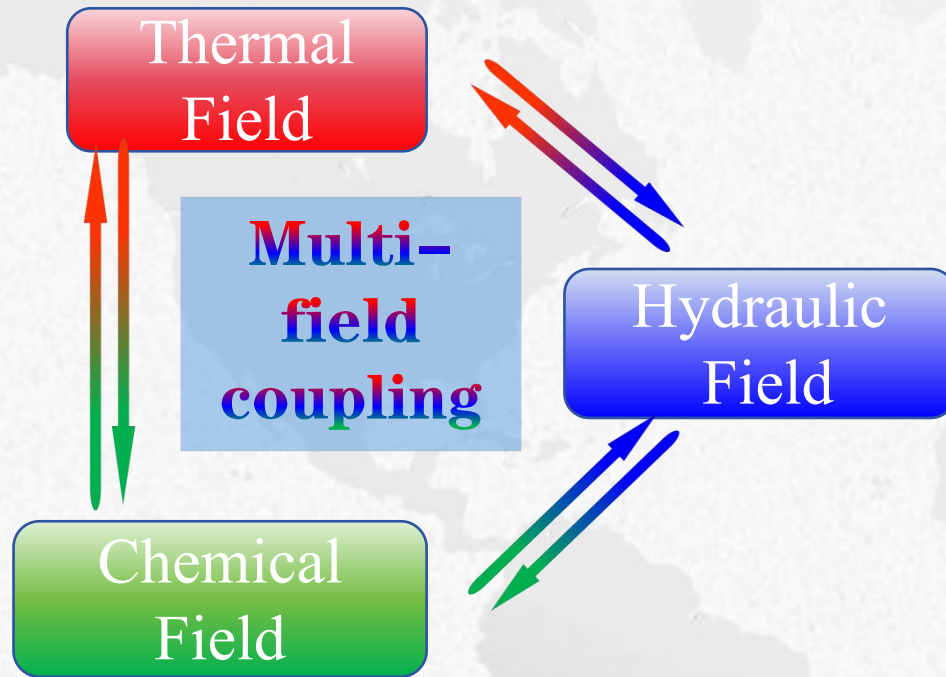
3. Theory and Methods



$$c\rho \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left(\lambda_x \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left(\lambda_y \frac{\partial T}{\partial y} \right) + \frac{\partial}{\partial z} \left(\lambda_z \frac{\partial T}{\partial z} \right) - \frac{\partial}{\partial x} (c_w \rho_w T \cdot u_x) - \frac{\partial}{\partial y} (c_w \rho_w T \cdot u_y) - \frac{\partial}{\partial z} (c_w \rho_w T \cdot u_z) + f$$

Thermal Transport Equation: ↑↑↑

$$\text{Heat Balance Equation: } (\rho c)_w \pi r_c^2 \frac{d(hT_*)}{dt} = 2\pi r_s \cdot \lambda M \left. \frac{dT}{dr} \right|_{r=r_s}$$



Groundwater Continuity Equation:

$$\mu_s \frac{\partial H}{\partial t} = \frac{\partial}{\partial x} (K_x \frac{\partial H}{\partial x}) + \frac{\partial}{\partial y} (K_y \frac{\partial H}{\partial y}) + \frac{\partial}{\partial z} (K_z \frac{\partial H}{\partial z})$$

$$\text{Water Balance Equation: } \pi r_c^2 \frac{dw}{dt} = 2\pi r_s \cdot T \left. \frac{\partial h}{\partial r} \right|_{r=r_s}$$

Solute Transport Equation: ↓↓↓

$$\text{Solute Balance Equation: } \pi r_c^2 \frac{d(hC_*)}{dt} = 2\pi r_s \cdot DM \left. \frac{dC}{dr} \right|_{r=r_s}$$

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left(D_x \frac{\partial C}{\partial x} \right) + \frac{\partial}{\partial y} \left(D_y \frac{\partial C}{\partial y} \right) + \frac{\partial}{\partial z} \left(D_z \frac{\partial C}{\partial z} \right) - \frac{\partial}{\partial x} (C \cdot u_x) - \frac{\partial}{\partial y} (C \cdot u_y) - \frac{\partial}{\partial z} (C \cdot u_z) + I$$



3. Theory and Methods

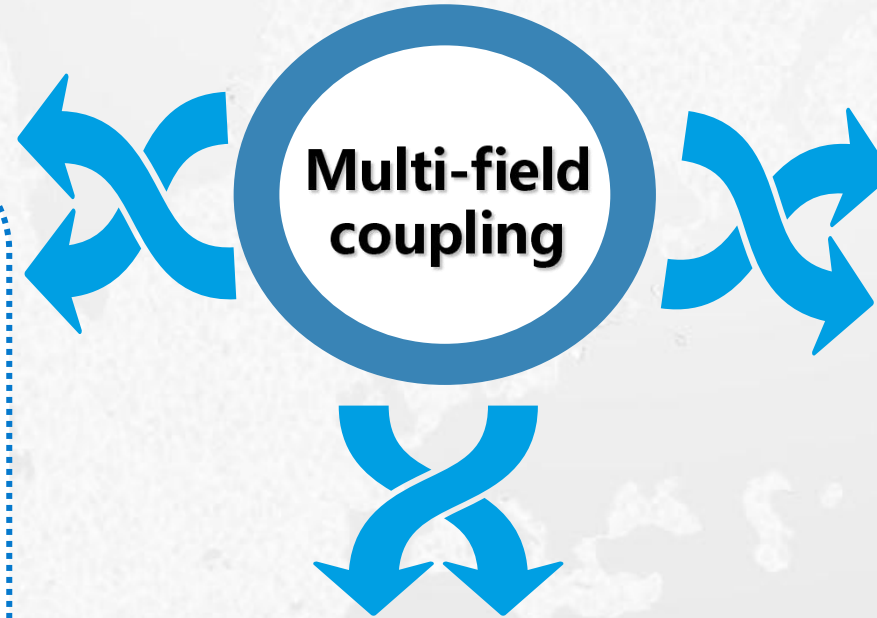


1. Hydraulic field

K : Hydraulic Conductivity

μ_s : Storage Coefficient

v : Darcy' s velocity



**Multi-field
coupling**

2. Thermal field

λ : Thermal Conductivity

ρ : Density

c : Heat Capacity

α_h : Thermal dispersivity

3. Chemical field

D_L : Dispersion Coefficient

**D_0 : Molecular Diffusion
Coefficient**

α_L : Dispersivity



3. Theory and Methods



Hydraulic Field

$$\begin{aligned}\mu_s \frac{\partial H}{\partial t} &= K \frac{\partial H}{\partial x^2} \\ H(x, 0) &= H_0 \\ H(L, t) &= H_0 \\ H(0, t) &= H_w(t) + H_0 \\ \frac{dH_w}{dt} &= K \frac{\partial H}{\partial x} \Big|_{x=0} \\ H_w(0) &= H_{w0} \\ v(x, t) &= -K \frac{\partial H}{\partial x}\end{aligned}$$

$$\begin{aligned}\mu_s \frac{\partial H}{\partial t} &= \frac{1}{r} \frac{\partial}{\partial x} \left(Kr \frac{\partial H}{\partial r} \right) \\ H(r, 0) &= H_0 \\ H(L, t) &= H_0 \\ H(0, t) &= H_w(t) + H_0 \\ \frac{dH_w}{dt} &= \frac{2bK}{r_w} \frac{\partial H}{\partial r} \Big|_{r=0} \\ H_w(0) &= H_{w0} \\ v(r, t) &= -K \frac{\partial H}{\partial r}\end{aligned}$$

One-dimensional sand column model

Chemical Field

$$\begin{aligned}\frac{\partial(nC)}{\partial t} &= \frac{\partial}{\partial x} \left(nD_x \frac{\partial C}{\partial x} - vC \right) \\ D_x &= D_0 + \alpha_{cx} \cdot \frac{v}{n} \\ C(x, 0) &= C_0 \\ C(L, t) &= C_0 \\ C(0, t) &= C_w(t) + C_0 \\ \frac{d[(H_w + H_0)(C_w + C_0)]}{dt} &= \left(nD_x \frac{\partial C}{\partial x} - vC \right) \Big|_{x=0} \\ C_w(0) &= C_{w0}\end{aligned}$$

$$\begin{aligned}\frac{\partial(nC)}{\partial t} &= \frac{1}{r} \frac{\partial}{\partial r} \left(nD_r r \frac{\partial C}{\partial r} \right) - \frac{1}{r} \frac{\partial(vrC)}{\partial r} \\ D_r &= D_0 + \alpha_{cr} \cdot \frac{v}{n} \\ C(r, 0) &= C_0 \\ C(L, t) &= C_0 \\ C(0, t) &= C_w(t) + C_0 \\ \frac{d[(H_w + H_0)(C_w + C_0)]}{dt} &= \frac{2b}{r_w} \left(nD_r \frac{\partial C}{\partial r} - vC \right) \Big|_{r=0} \\ C_w(0) &= C_{w0}\end{aligned}$$

Thermal Field

$$\begin{aligned}(\rho c)_f \frac{\partial T}{\partial t} &= \frac{\partial}{\partial x} \left[\lambda_x \frac{\partial T}{\partial x} - (\rho c)_f vT \right] \\ \lambda_x &= \lambda_p + \lambda_{vx} \\ \lambda_p &= (\rho c)_f s \left[n \frac{\lambda_f}{(\rho c)_f} + (1-n) \frac{\lambda_s}{(\rho c)_s} \right] \\ \lambda_p &= n\lambda_f + (1-n)\lambda_s \\ \lambda_{vx} &= \alpha_{hx} (\rho c)_f v \\ T(x, 0) &= T_0 \\ T(L, t) &= T_0 \\ T(0, t) &= T_w(t) + T_0 \\ (\rho c)_f \frac{d[(H_w + H_0)(T_w + T_0)]}{dt} &= \left[\lambda_x \frac{\partial T}{\partial x} - (\rho c)_f vT \right] \Big|_{x=0} \\ T_w(0) &= T_{w0}\end{aligned}$$

$$\begin{aligned}(\rho c)_f \frac{\partial T}{\partial t} &= \frac{1}{r} \frac{\partial}{\partial x} \left[\lambda_r r \frac{\partial T}{\partial r} - (\rho c)_f vrT \right] \\ \lambda_x &= \lambda_p + \lambda_{vr} \\ \lambda_p &= (\rho c)_f s \left[n \frac{\lambda_f}{(\rho c)_f} + (1-n) \frac{\lambda_s}{(\rho c)_s} \right] \\ \lambda_p &= n\lambda_f + (1-n)\lambda_s \\ \lambda_{vr} &= \alpha_{hr} (\rho c)_f v \\ T(r, 0) &= T_0 \\ T(L, t) &= T_0 \\ T(0, t) &= T_w(t) + T_0 \\ (\rho c)_f \frac{d[(H_w + H_0)(T_w + T_0)]}{dt} &= \frac{2b}{r_w} \left[\lambda_r \frac{\partial T}{\partial r} - (\rho c)_f vrT \right] \Big|_{r=0} \\ T_w(0) &= T_{w0}\end{aligned}$$

two-dimensional well flow model



3. Theory and Methods



Well-posed Problem

Dimensionless Factors

$$\begin{cases} \frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2} & 0 < x < L, t > 0 \\ T(x, 0) = T_0 & 0 < x < L \\ T(L, t) = T_0 & t \geq 0 \\ T(0, t) = T_A + T_0 & t \geq 0 \end{cases}$$

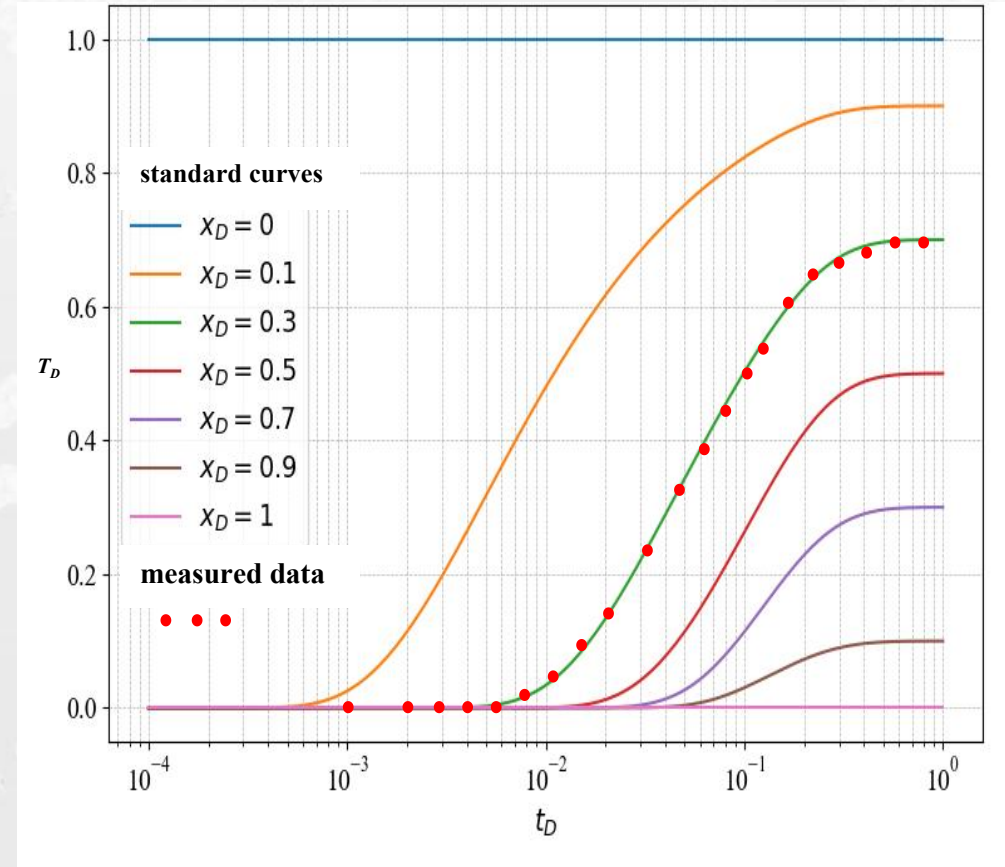
$$\begin{cases} x_D = \frac{x}{L} \\ T_D = \frac{T - T_0}{T_A} \\ t_D = \frac{D_0 t}{L^2} \end{cases}$$

Separation of Variables

$$T_D(x_D, t_D) = (1 - x_D) - \sum_{n=1}^{\infty} \frac{2}{n\pi} e^{-(n\pi)^2 t_D} \sin(n\pi x_D)$$

$$T(x, t) = T_0 + T_A \left[\left(1 - \frac{x}{L} \right) - \sum_{n=1}^{\infty} \frac{2}{n\pi} e^{-(n\pi)^2 \frac{D_0 t}{L^2}} \sin\left(\frac{n\pi x}{L}\right) \right]$$

Analytical Solution





3. Theory and Methods



Well-posed Problem

$$\begin{cases} \mu^* \frac{\partial H}{\partial t} = \frac{\partial^2 H}{\partial r^2} + \frac{1}{r} \frac{\partial H}{\partial r} & r_s < r < r_L, t > 0 \\ H(r, 0) = H_0 & r_s < r \leq r_L \\ H(r_L, t) = H_0 & t > 0 \\ H(r_s, t) = w(t) + H_0 & t \geq 0 \\ \pi r_c^2 \frac{dw}{dt} = 2\pi r_s T \frac{\partial H}{\partial r} \Big|_{r=r_s} & t \geq 0 \\ w(0) = w_0 & t = 0 \end{cases}$$

Dimensionless Factors

$$\begin{cases} r_D = \frac{r}{r_s} \\ r_{LD} = \frac{r_L}{r_s} \\ H_D = \frac{H - H_0}{w_0} \\ w_D = \frac{w}{w_0} \\ t_D = \frac{Tt}{r_c^2} \\ \mu_D^* = \frac{r_s^2}{r_c^2} \mu^* \\ s^* = \sqrt{\mu_D^*} s \end{cases}$$



Dimensionless Transformation

$$\begin{cases} \mu_D^* \frac{\partial H_D}{\partial t_D} = \frac{\partial^2 H_D}{\partial r_D^2} + \frac{1}{r_D} \frac{\partial H_D}{\partial r_D} & 1 < r_D < r_{LD}, t_D > 0 \\ H_D(r_D, 0) = 0 & 1 \leq r_D \leq r_{LD} \\ H_D(r_{LD}, t_D) = 0 & t_D > 0 \\ H_D(1, t_D) = w_D(t_D) & t_D \geq 0 \\ \frac{dw_D}{dt_D} = 2 \frac{\partial H_D}{\partial r_D} \Big|_{r_D=1} & t_D \geq 0 \\ w_D(0) = 1 \end{cases}$$

**Laplace
Transform**



Frequency Domain Solution

$$\bar{w}_D(s) = \frac{1}{s + 2s^* \frac{I_0(s^* r_{LD}) K_1(s^*) + I_1(s^*) K_0(s^* r_{LD})}{I_0(s^* r_{LD}) K_0(s^*) - I_0(s^*) K_0(s^* r_{LD})}}$$

$$\tilde{H}_D(r_D, s) = \frac{K_0(s^* r_D) I_0(s^* r_{LD}) - K_0(s^* r_{LD}) I_0(s^* r_D)}{K_0(s^*) I_0(s^* r_{LD}) - K_0(s^* r_{LD}) I_0(s^*)} \bar{w}_D(s)$$

Semi-analytical Solution



3. Theory and Methods



Laplace Inverse Transform

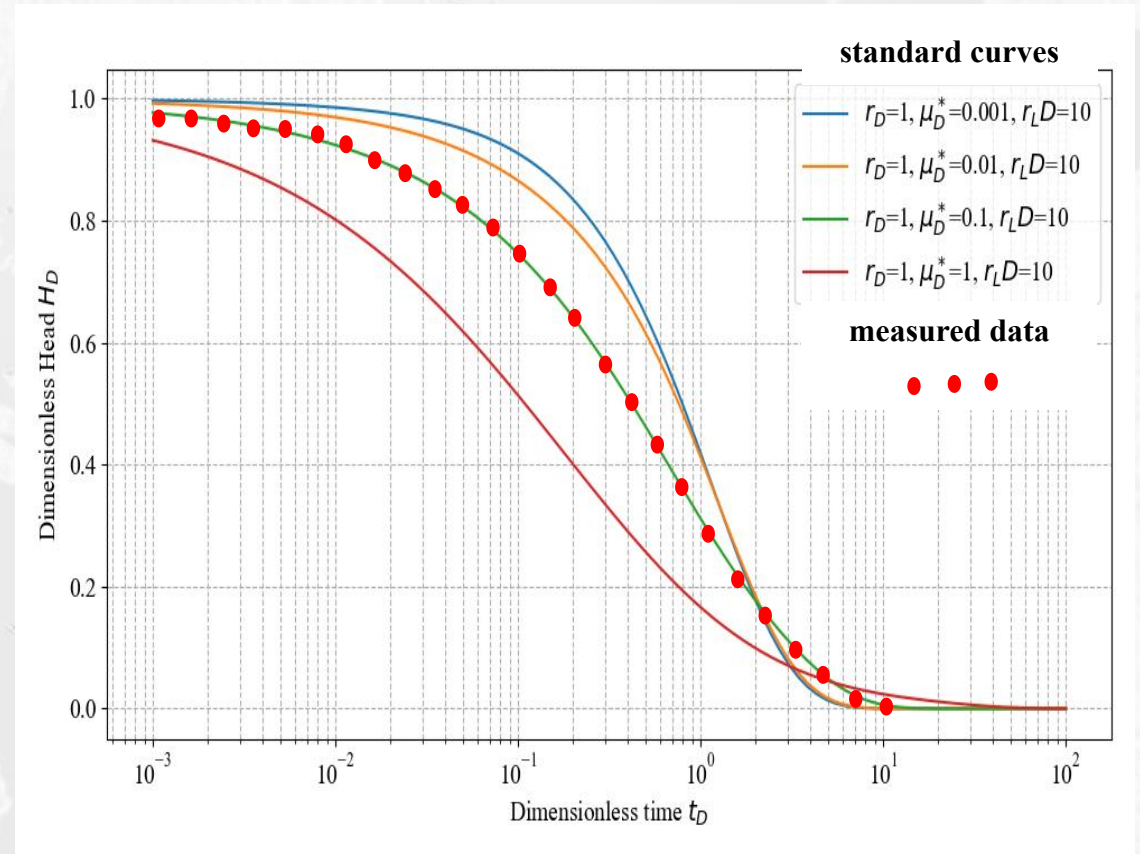


Stehfest Method

$$w_D(t_D) \approx \frac{\ln 2}{t_D} \sum_{n=1}^N V_n \bar{w}_D \left(\frac{n \ln 2}{t_D} \right)$$

$$V_n = (-1)^{n+N/2} \sum_{k=[(n+1)/2]}^{\min(n, N/2)} \frac{k^{N/2} (2k)!}{(N/2 - k)! k! (k-1)! (n-k)! (2k-n)!}$$

Semi-analytical Solution





3. Theory and Methods



Well-posed Problem

$$\left\{ \begin{array}{l} \mu_s \frac{\partial H}{\partial t} = K \frac{\partial^2 H}{\partial x^2} \\ H(x, 0) = H_0 \\ H(L, t) = H_0 \\ H(0, t) = w(t) + H_0 \\ \left. \frac{dw}{dt} = K \frac{\partial H}{\partial x} \right|_{x=0} \\ w(0) = w_0 \\ u(x, t) = -\frac{1}{n} K \frac{\partial H}{\partial x} \\ \frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left(D_L \frac{\partial C}{\partial x} \right) - \frac{\partial}{\partial x} (uC) \\ D_L = D_0 + \alpha_L u \\ C(x, 0) = C_0 \\ C(L, t) = C_0 \\ C(0, t) = C_w(t) + C_0 \\ \left. \frac{d[(w+h_0) \cdot (C_w + C_0)]}{dt} = n \left(D_L \frac{\partial C}{\partial x} - uC \right) \right|_{x=0} \\ C_w(0) = C_{w0} \end{array} \right.$$

Dimensionless Factors

$$\left\{ \begin{array}{l} H_0 = \frac{H - H_0}{w_0} \\ x_D = \frac{x}{L} \\ C_D = \frac{C - C_0}{C_{w0}} \\ w_D = \frac{w}{w_0} \\ C_{wD} = \frac{C_w}{C_{w0}} \\ t_D = \frac{Kt}{L} \\ \mu_{sD} = \mu_s L \\ C_{0D} = \frac{C_0}{C_{w0}} \\ D_{LD} = \frac{D_L}{KL} \\ u_D = \frac{u}{K} \\ D_{0D} = \frac{D_0}{KL} \\ Pe = \frac{\alpha_L}{L} \\ h_{0D} = \frac{h_0}{w_0} \\ n_D = \frac{nL}{w_0} \end{array} \right.$$



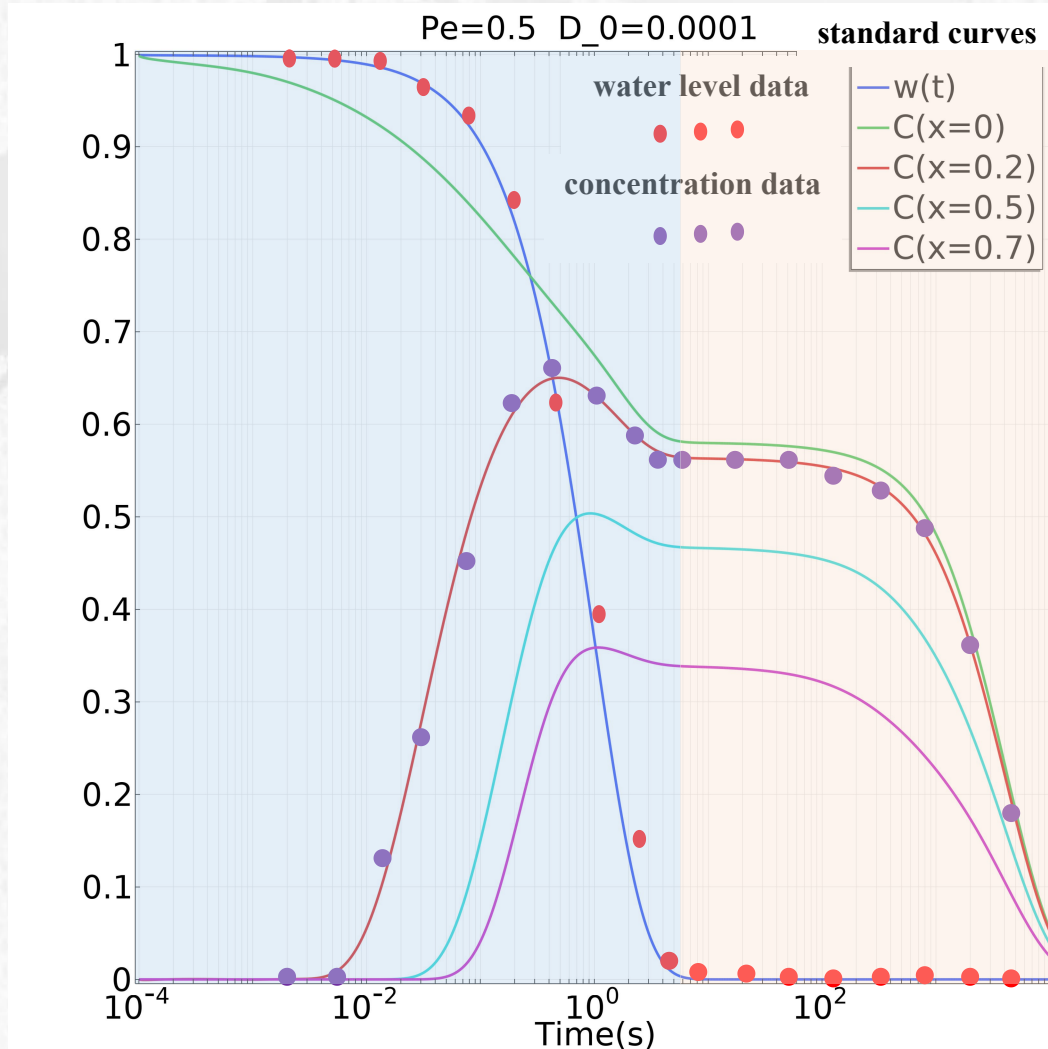
Dimensionless Transformation

$$\left\{ \begin{array}{l} \mu_{sD} \frac{\partial H_D}{\partial t_D} = \frac{\partial^2 H_D}{\partial x_D^2} \\ H_D(x_D, 0) = 0 \\ H_D(L, t_D) = 0 \\ H_D(0, t_D) = w_D(t_D) \\ \left. \frac{dw_D}{dt_D} = \frac{\partial H_D}{\partial x_D} \right|_{x_D=0} \\ w_D(0) = 1 \\ u_D = -\frac{1}{n_D} \frac{\partial H_D}{\partial x_D} \\ \frac{\partial C_D}{\partial t_D} = \frac{\partial}{\partial x_D} \left[D_{LD} \frac{\partial C_D}{\partial x_D} - u_D (C_{0D} + C_D) \right] \\ D_{LD}(u_D) = D_{0D} + Pe u_D \\ C_D(x_D, 0) = 0 \\ C_D(L, t_D) = 0 \\ C_D(0, t_D) = C_{wD}(t_D) \\ C_{wD}(0) = 1 \\ \left. \frac{d[(w_D + h_{0D}) C_{wD}]}{dt_D} = n_D \left[D_{LD} \frac{\partial C_D}{\partial x_D} - u_D (C_{0D} + C_D) \right] \right|_{x_D=0} \end{array} \right.$$

Numerical Solution (COMSOL)



3. Theory and Methods



**Hydraulic
Control**

**Molecular
Diffusion
Control**

$$\left\{ \begin{array}{l} K = \frac{[t_D]L}{[t]} \\ \mu_s = \frac{[\mu_{sD}]}{L} \\ \alpha_L = [Pe]L \\ D_0 = [D_{0D}]KL \\ D_L = D_0 + \alpha_L u \end{array} \right.$$

Multiple hydrogeological parameters can be calculated simultaneously by matching data from multiple fields in a single test

Numerical Solution (COMSOL)



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Conclusion



4. Conclusion



1. Coupled Model Validation

Combined experiments and simulations validate coupled hydraulic-thermal-solute models for reliable estimation of permeability, thermal conductivity, and dispersion coefficients.

2. Enhanced Parameter Accuracy

Synergistic experimental-numerical approaches improve parameter identification in multi-physics systems, resolving complex coupling mechanisms.

3. Robust Experimental Framework

High-precision laboratory measurements and cross-validation quantify spatiotemporal dynamics of coupled flow, heat, and solute transport.

Analytical solution+Indoor experiments+Numerical simulation



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your time and attention

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